Sao Paulo, Brazil, 18-20 May 2011 - Paulista University 3rd International Workshop "Advances in Cleaner Production"



Organic Waste, Residues and By-Products from Agricultural, Industrial and Urban Systems as Biorefinery Substrates. Viable Option or Fairie Tales? An Application of SUMMA (SUstainability Multi-method Multi-scale Assessment)

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Contributors:

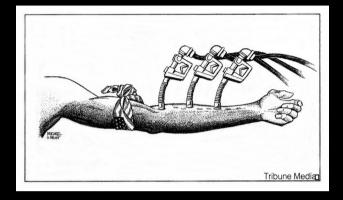
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A Problem - Us

- All studies clearly identify human activity as a primary cause of the Earth System Crisis
- The 20th Century has seen exponential growth in human populations, made possible by the industrial-scale exploitation of natural resources and services
- The globalised industrial economy is committed to continuing growth in production and consumption
- Growth demands ever-increasing energy and material inputs
- Growth results in increasing levels of pollution, resource depletion, species loss and ecosystem degradation.

Business-as-usual

Advocates of business-as-usual suggest that what is needed to maintain a growing economy is increased efforts to extract more energy from deeper reservoirs, oil sands, nuclear.



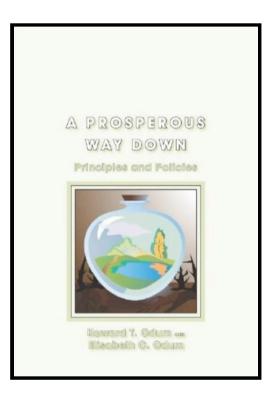
They disregard the declining net return of these sources (increased efforts mean increased energy investment, less net energy, more environmental disturbance).



Business-as-usual is not an option for the future of humankind.

Unlimited growth is impossible in a limited planet and sooner or later every activity is constrained by a limiting factor. Howard T. Odum (1925-2002): the impossibility of business-as-usual and the search for alternatives.





Howard T. Odum and Elisabeth C. Odum (2001) A Prosperous Way Down: Principles and Policies.

Boulder, Colorado: University Press of Colorado.

Main premises of cleaner production and sustainable societies:

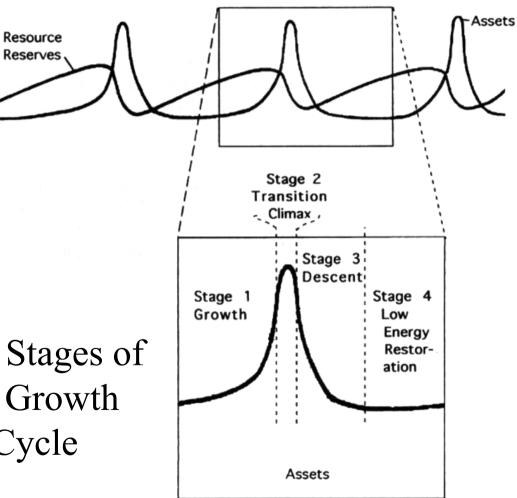
a) recognizing the stage we are in;

b) Choosing the appropriate policy for that stage.

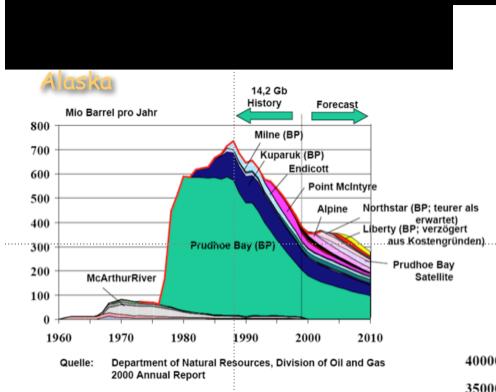
c) Growth policies do not fit descent periods

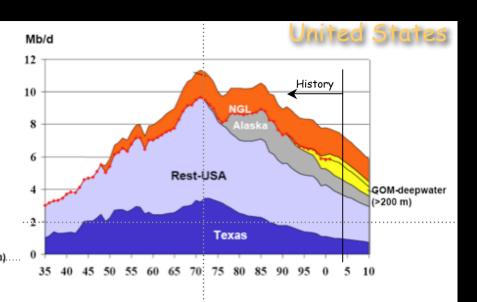
Four Stages of the Growth Cycle

Odum's Pulsing Model

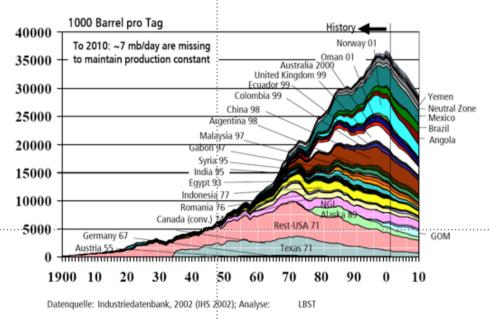


Time



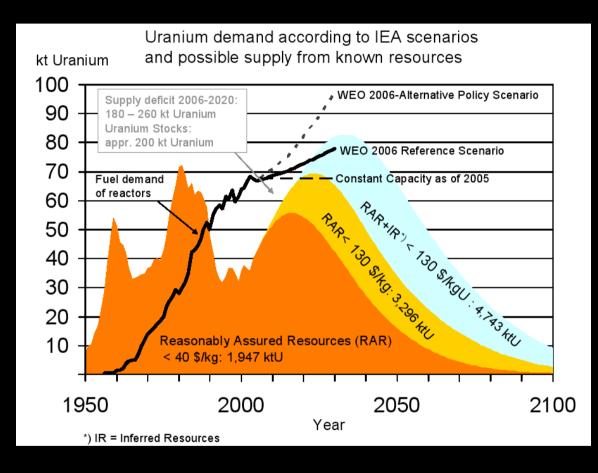


e: Texas Railroad Commission US Energy Information Administration



No matter how you cut it...the hydrocarbon age (cheap fossil fuels) is over.

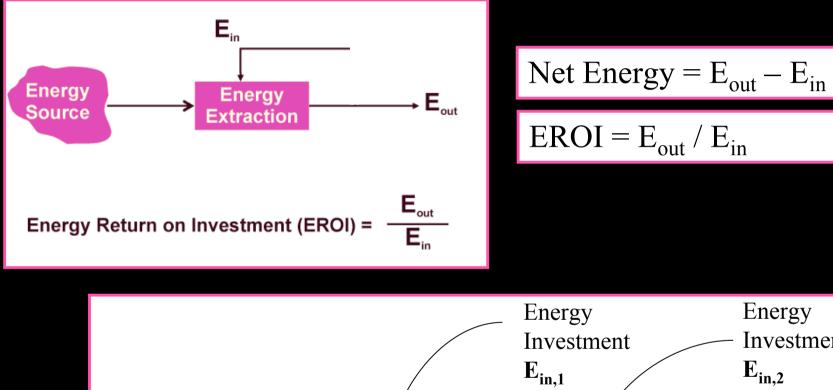
A PEAK FOR (CHEAP) URANIUM ?



Estimates of available uranium stocks at different price compared to the present uranium demand for existing reactors

Source: EWG, 2006. URANIUM RESOURCES AND NUCLEAR ENERGY. Energy Watch Group, December 2006. EWG-Series No.1/2006. http://www.energywatchgroup.org/fileadmin/global/pdf/EWG_Report_Uranium_3-12-2006ms.pdf.

Net Energy and EROI (Energy Return on Investment)



E_{in}

Resource in

the ground

Refined

resource

Eout

Refining

process

Extracted

resource

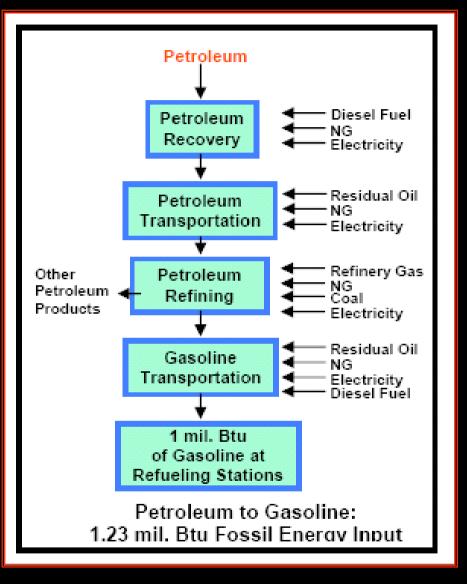
Extraction

process

Fossil oil to gasoline process

(Michael Wang, 2005, Ethanol from Corn and Cellulosics, Center for Transportation Research, Argonne National Laboratory)

The EROI of refined fuels is around 5:1



The search for alternatives

Our addiction to fossil fuels results on intensive consumption of petroleum derivatives which, combined with diminishing petroleum resources, causes environmental and political concerns.

Electricity and heat can be provided by a variety of renewable alternatives (wind, sun, hydro, geo, and so on).

Instead, the fossil resource alternative for production of transportation fuels and chemicals is biomass, the only C-rich material source available on the Earth, besides fossils.

Alternatives must be:

A) Environmentally friendly: less, or no loading at all on water, land, air, climate, biodiversity.

B) Renewable. The age of fossil fuels is over.

C) Complex and integrated: components interact and exchange energy and matter flows in order to decrease emissions and waste.

D) Aiming at wellbeing, not at growth.

E) Sustainable under different points of view: energetic, environmental, economic, and social.

Bio-ethanol production in the contaminated land around Chernobyl (Belarus)?



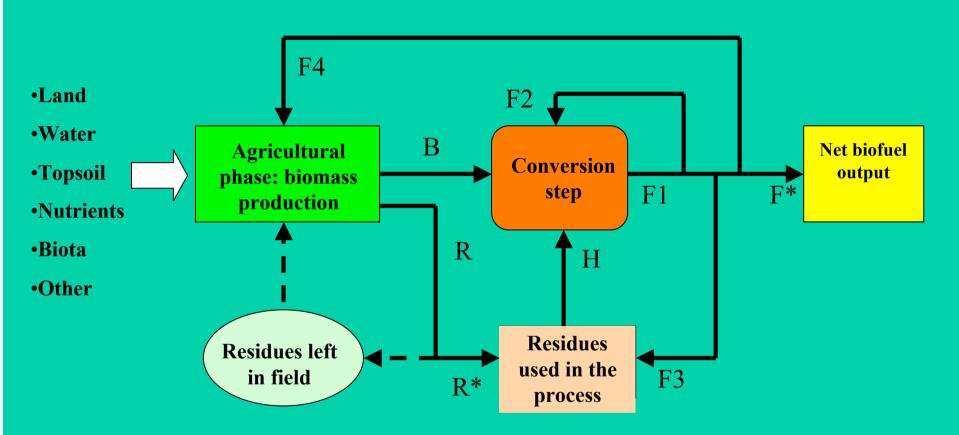


In 2009 an Irish Company (Greenfield Project Management Ltd) planned to use four million ha in Belarus, in the Chernobyl surroundings. The biofuel produced should have been commercialised in Europe. This was a false annoucement to raise money in order to avoid bankrupcy (<u>http://www.facebook.com/note.php?note_id=145364802189057</u>).

On 16 May 2011, PhotoFuels, a Belgian-Ukrainian joint venture, announced to have obtained approval from the Ukraine government to plant several test fields of common millet for biofuels in the Chernobyl area evacuated in the year 1986 after the nuclear power accident. (Deutsche Presse-Agentur)

The failure of Bioenergy from food crops: corn, wheat, oilseeds,...

Biofuel Production



- **F1 = Gross biofuel production**
- **F2** = **Process energy demand met by biofuels**
- **F3** = Biofuels invested in harvesting of residues
- **F4** = **Biofuel demand for agricultural production**

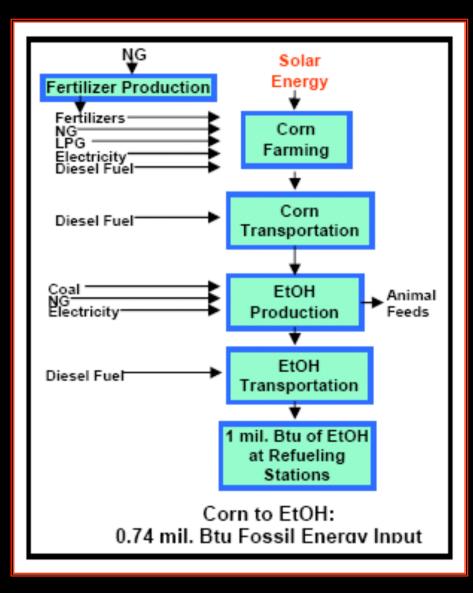
R = Potentially available residues (mass)

- **R*** = **Residues used in process (mass)**
- **H** = **Process energy demand met by residues**
- **B** = Total biomass produced (mass)

Corn to EtOH process

(Michael Wang, 2005, Ethanol from Corn and Cellulosics, Center for Transportation Research, Argonne National Laboratory)

The EROI of bioethanol from corn is around 1.3:1



	Units	Wheat	Com
Energy and mass flows			
Total commercial energy invested for grain production	J/ha/yr	2,38E+10	2.92E+10
Total commercial energy invested for bioethanol production	J/ha/yr	3.28E+10	4.92E+10
Grain produced	g/ha/yr	4.30E+06	7.60E+06
Ethanol produced	g/ha/yr	1,20E+06	1,96E+06
Energy content of bioethanol produced	J/ha/yr	3.57E+10	5.84E+10
Net energy yield of bioethanol (energy of ethanol-energy invested)	J/ha/yr	2.89E+09	9.15E+09
Ethanol production Energy cost of ethanol Output/input energy ratio	J/g	2.74E+04 1.09	2.51E+04 1.19
Transformity of ethanol, with labor and services	seJ/J	2.77E+05	1.89E+05
Transformity of ethanol, without labor and services	seJ/J	1.675+65	1,245+05

Energy and eMergy evaluation of bioethanol production from wheat in Henan Province, China

Xiaobin Dong^a, Sergio Ulgiati^b, Maochao Yan^{c,d}, Xinshi Zhang^a, Wangsheng Gao^{c,*}

Energy Policy 36 (2008) 3882-3892

Second Generation vs First Generation? Maybe...

• 1st generation biofuels

Derived from Biomass harvested for the sugar, starch and oil content, which can be converted using hydrolysis & fermentation

Technology established

Major Issues - Crops needed, Food v Fuel, Water Demand, Environmental issues - land clearing, soil degradation.

• 2nd generation biofuels

Produced from lignocellulosic biomass, utilising hydrolysis, fermentation, gasification or pyrolysis

Can utilise Waste Materials (e.g. waste paper, paper mill waste, wood waste, agricultural crop residues etc)

Table 5 Energy and emergy performance indicators for bioethanol production for each pretreatment system

lterer.	Unit	Pretreatment system					
Item		Dilute acid	Controlled pH	Flowthrough	AFEX	ARP	Lime
Energy and mass flows							
Total energy invested for bioethanol production	J	1.93E+13	7.48E+12	4.48E+13	8.31E+12	1.06E+13	2.22E+12
Mass of bioethanol and co-products produced	g	3.57E+08	3.07E+08	3.82E+08	2.56E+08	3.07E+08	2.36E+08
Energy content of bioethanol and co-products produced	J	1.06E+13	9.13E+12	1.14E+13	7.61E+12	9.15E+12	7.02E+12
Net energy yield	1	-8.67E+12	1.65E+12	-3.34E+13	-7.06E+11	-1.44E+12	4.81E+12
Emergy flows							
Locally renewable inputs, R	seJ	4.09E+17	4.09E+17	4.09E+17	4.09E+17	4.09E+17	4.09E+17
Locally nonrenewable inputs, N	seJ	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
% renewable of purchased inputs, %R_F	seJ	1.04E+16	8.22E+15	1.38E+16	1.02E+16	8.45E+15	1.01E+16
% nonrenewable of purchased inputs, %N_F	seJ	3.21E+18	1.37E+18	5.54E+18	7.13E+18	6.04E+18	1.19E+18
% renewable of Labor and Services, %R_S	seJ	6.32E+16	5.55E+16	6.70E+16	4.76E+16	5.55E+16	4.46E+16
% nonrenewable of Labor and Services, %N_S	seJ	1.80E+17	1.58E+17	1.91E+17	1.35E+17	1.58E+17	1.27E+17
Imported emergy, F = %R_F+%N_F+%R_S+%N_S	seJ	3.47E+18	1.59E+18	5.81E+18	7.33E+18	6.26E+18	1.37E+18
Total emergy inputs, Y = R+N+F	seJ	3.88E+18	2.00E+18	6.22E+18	7.74E+18	6.67E+18	1.78E+18
Bioethanol production			\frown				
Output/input energy ratio		0.55	1.22	0.25	0.92	0.86	3.17
Transformity of bioethanol, with co-product	seJ/J	3.65E+05	2.19E+05	5.47E+05	1.02E+06	7.29E+0	2.53E+05
EYR = Y/F		1.12	1.26	1.07	1.06	1.07	1.30
ELR = (N+F)/R		8.48	3.89	14.20	17.91	15.30	3.35
% Renewable = 1/(1+ELR) = R/Y		10.55%	20.47%	6.58%	5.29%	6.13%	23.00%
ESI = EYR/ELR		0.13	0.32	0.08	0.06	0.07	0.55

(Li et al., 2010; Wyman et al., 2005)

What is a biorefinery?

Biorefinery: the sustainable processing of biomass into a spectrum of marketable products and energy"

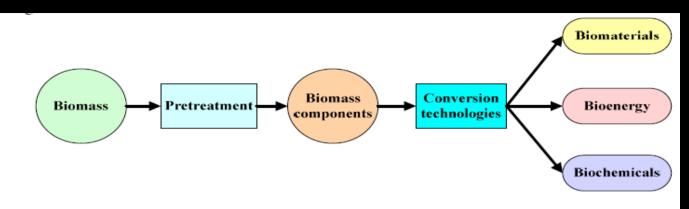


The "biorefinery" concept embraces a wide range of technologies able to separate biomass resources (wood, grasses, corn, urban waste) into their building blocks (carbohydrates, proteins, biogas, fats)...

...that can be converted to value added products, biofuels and chemicals.



In short:



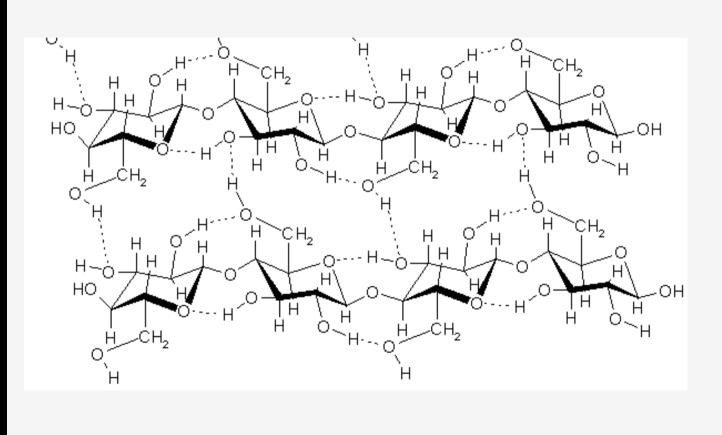
Simplified scheme of biorefinery: conversion of biomass into bioproducts.

Table 1-Most common biorefinery platforms and their major characteristics

Platform	Raw materials	Main processes	Products	Development stage
Sugar (Biochemical)	Lignocellulosic and starch biomass	Chemical and enzymatic hydrotysis, Fermentation, Biotransformation, Chemical and catalytical processes	Added value chemicals (both from sugar and lignin) Building block chemicals Materials (from lignin or lignocellulose) Fuel ethanol. Heat and electricity (from lignin)	Laboratory, large scale pilot plant and commercial (sugarcane and starch based)
Syngas (Thermochemical)	Lignocellulosic biomass but also plastics, rubber etc.	Thermochemical processes : - Gasification - Pyrolysis	Syngas Pyrotysis oil Added vatue chemicats Gaseous or tiquid fuets	Laboratory, large scale pilot plant
Biogas	Liquid effluents Manure	Anaerobic digestion	Methane and carbon dioxide (biogas) Added value chemicals	Large scale pilot plant, commercial
Carbon-rich chains (Oil)	Plant oils such as soybean, rapeseed corn, palm, and canola oils. Animal fat	Transesterification	Fatty acid methyl ester (biodiesel), Glycerin and fatty acids as platform chemicals	Commercial

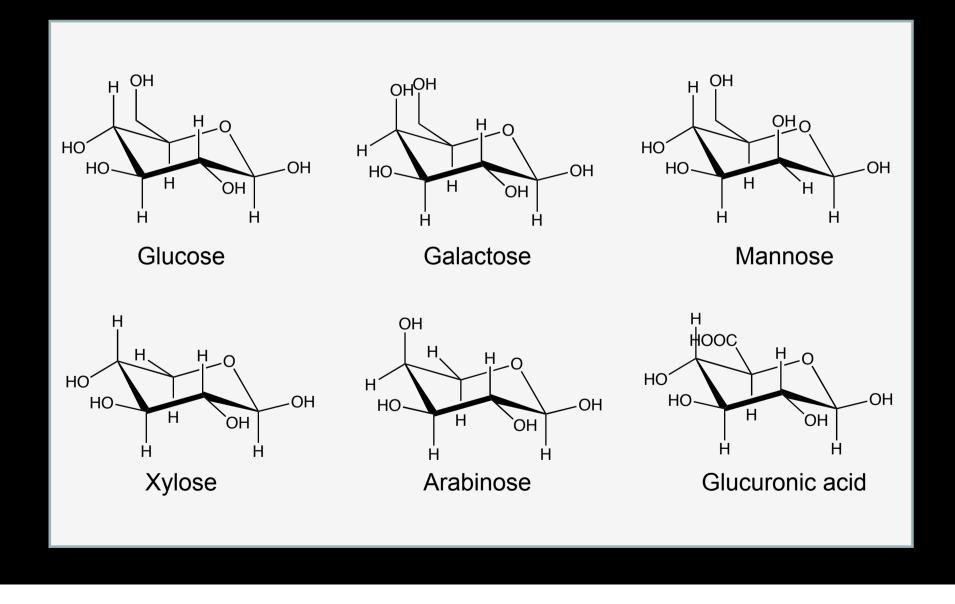
CELLULOSE

Extensive intramolecular and intermolecular H-bonding
Insoluble in water and most common organic solvents

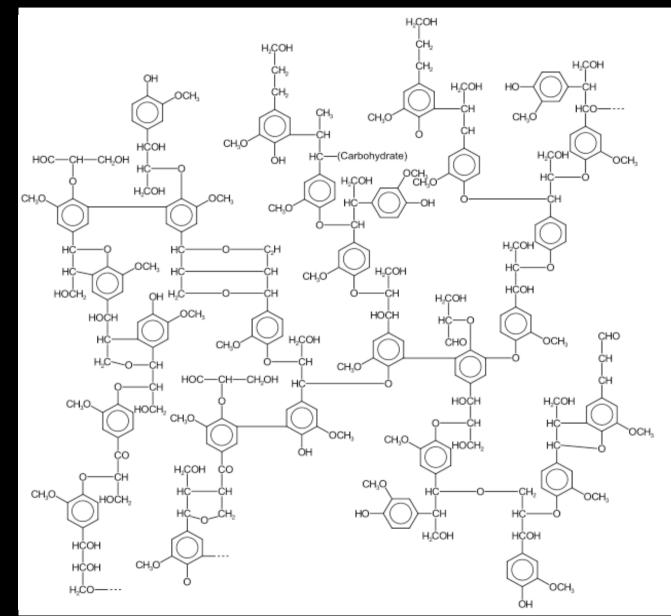


http://www.doitpoms.ac.uk/tlplib/wood/printall.php accessed on 9/03/09

HEMICELLULOSE

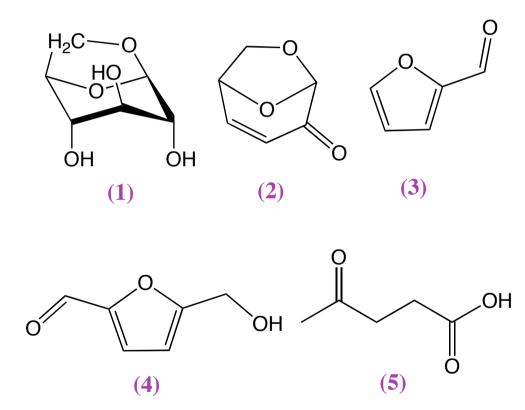


LIGNIN



http://commons.wikimedia.org/wiki/Image:Lignin_structure.svg?uselang=ja accessed on 9/03/09

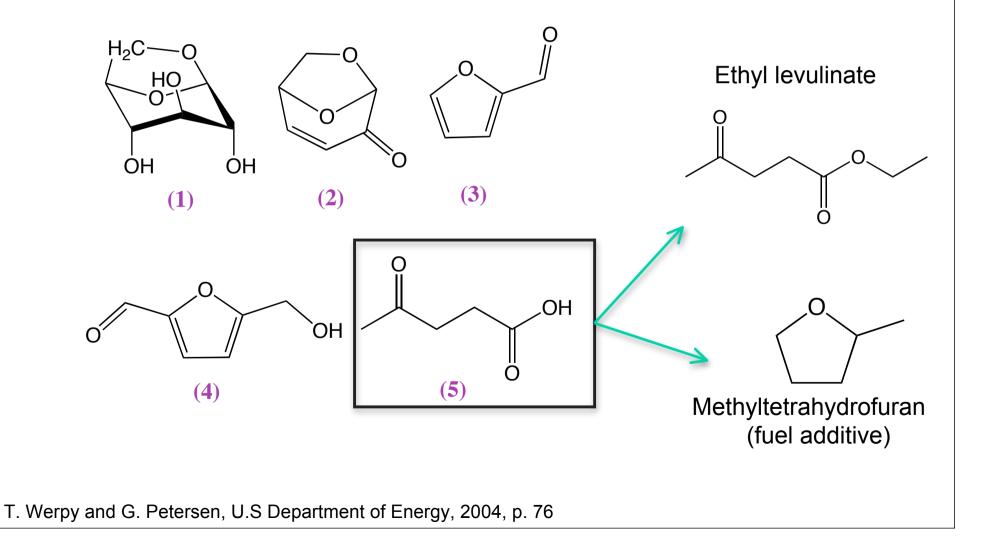
Chemical products from ligno-cellulosic materials

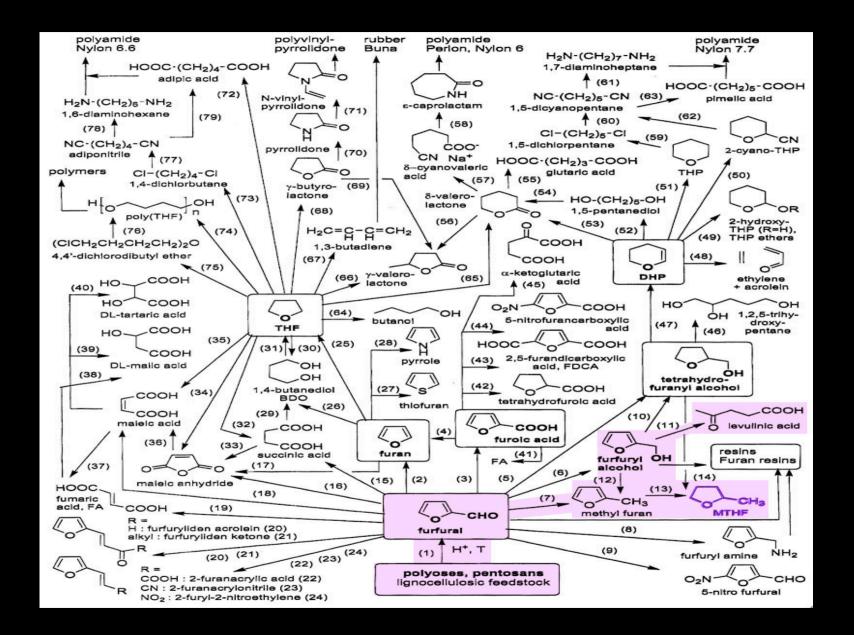


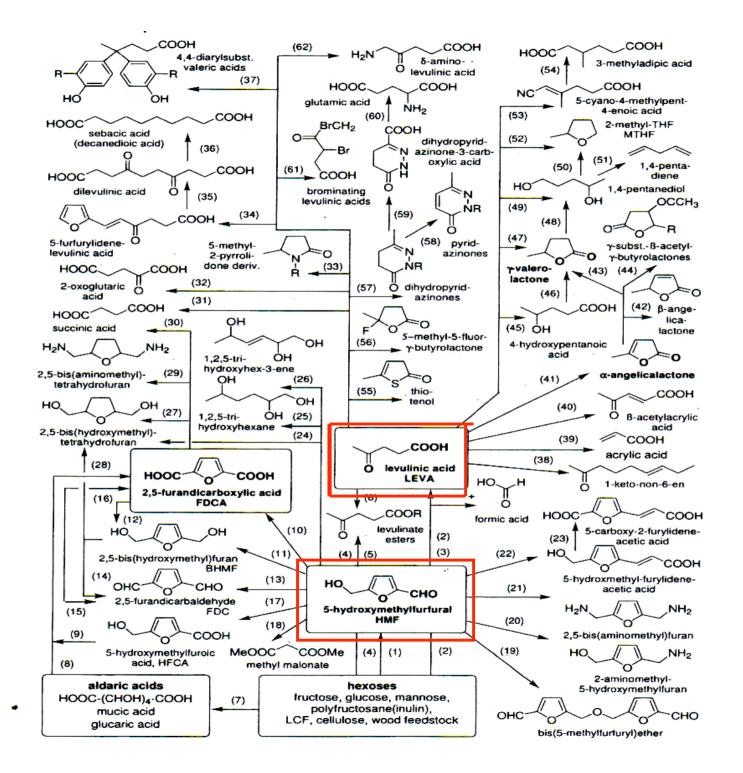
- 1. Levoglucosan
- 2. Levoglucosenone
- 3. Furfural
- 4. 5-Hydroxymethylfurfural
- 5. Levulinic acid

F. Shafizadeh and Y. L. Fu, *Carbohydr. Res., 1973, 29, 113-122.* R. Krishna, M. R. Kallury, C. Ambridge and T. T. Tidwell, *Carbohydr. Res., 1986, 158, 253-261* J. Horvat, B. Klaic, B. Metelko and V. Suniic, *Tetrahedron Lett*, 1985, 26, 2111-2114

Chemical products from ligno-cellulosic materials





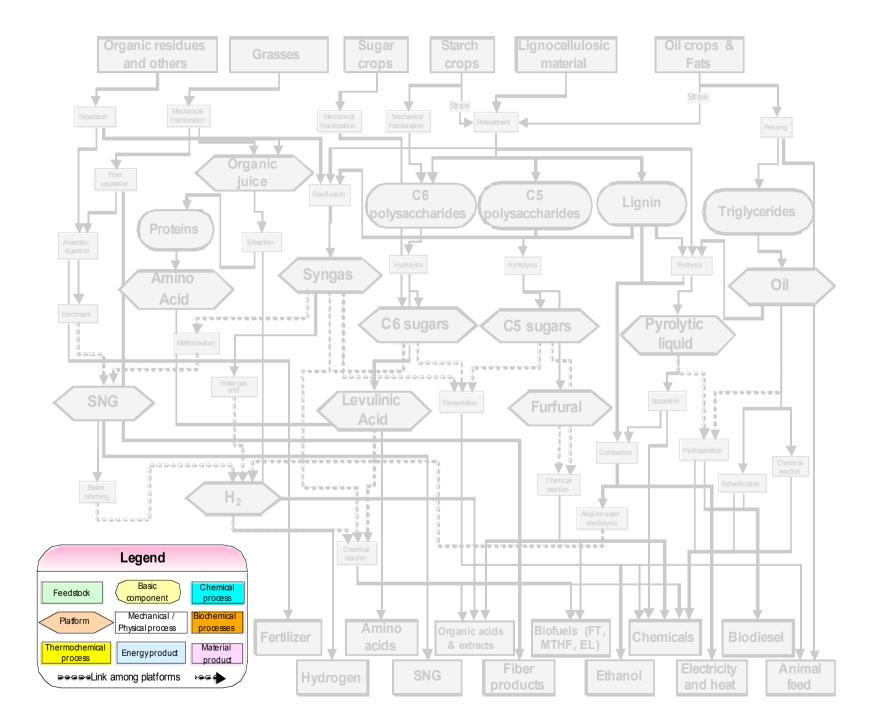


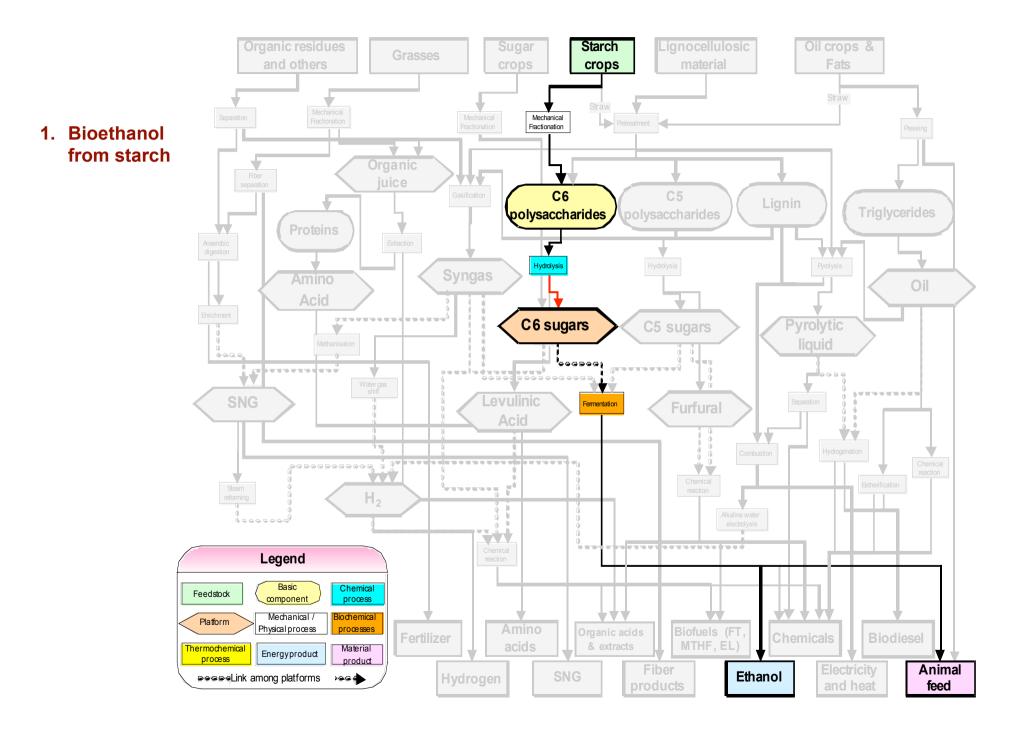
Levulinic Acid Derivatives

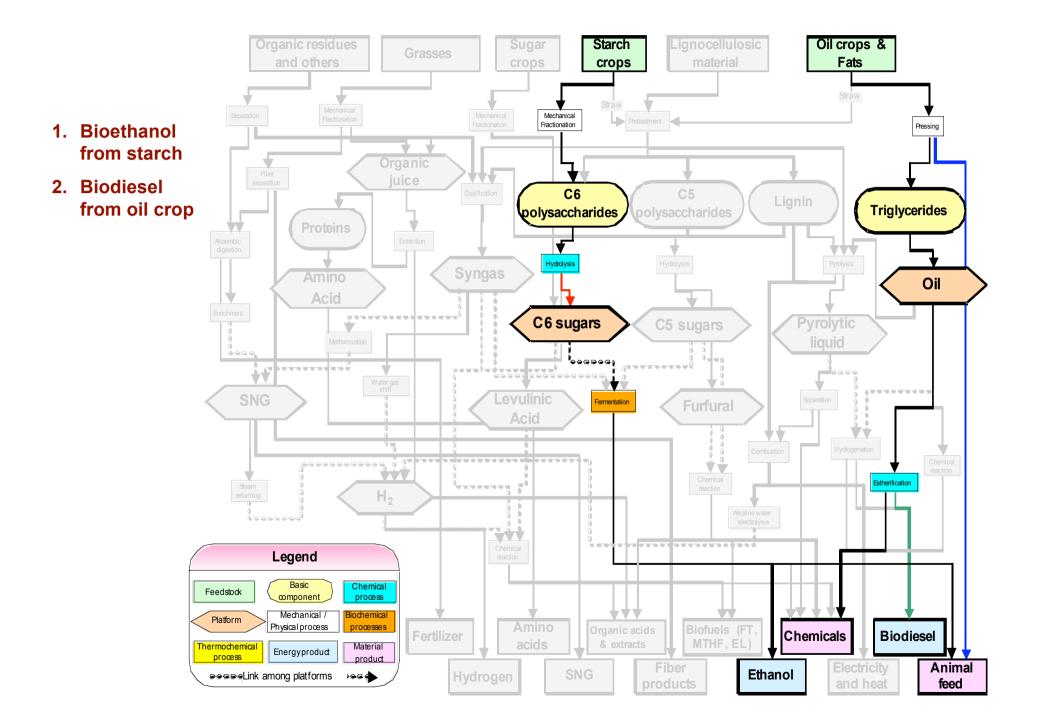
P.R. Gruber & M Kamm (Editors), "Biorefineries – Industrial Processes and Products, Status Quo and Future Directions, Vols 1 & 2, 2006, Wiley-VCH

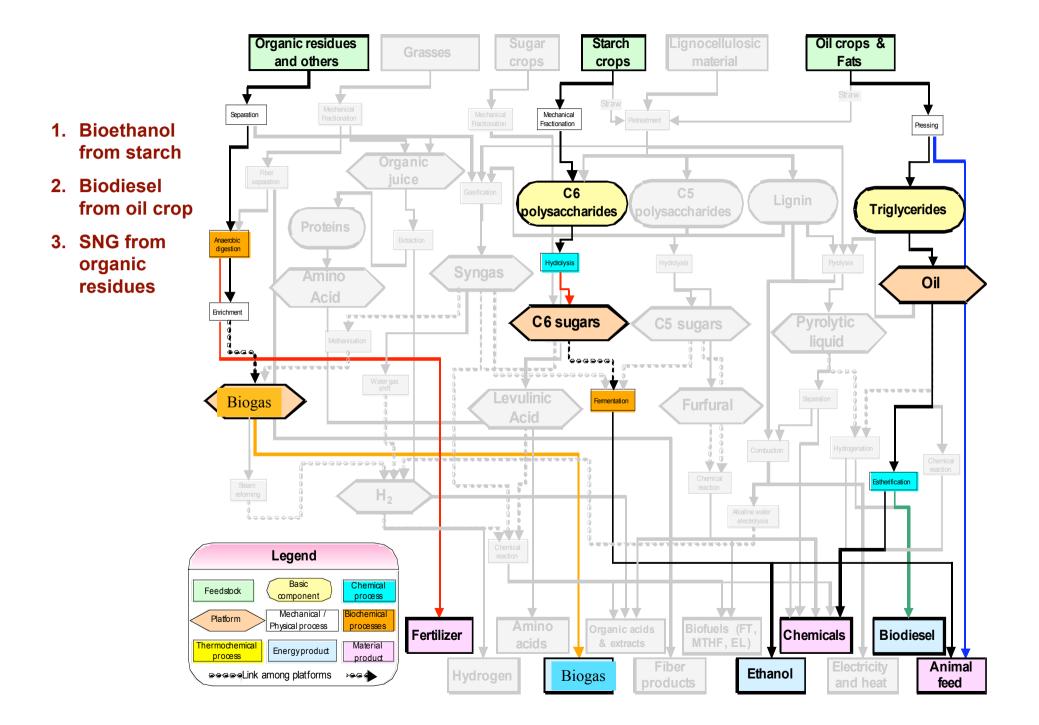
Step No. 1:

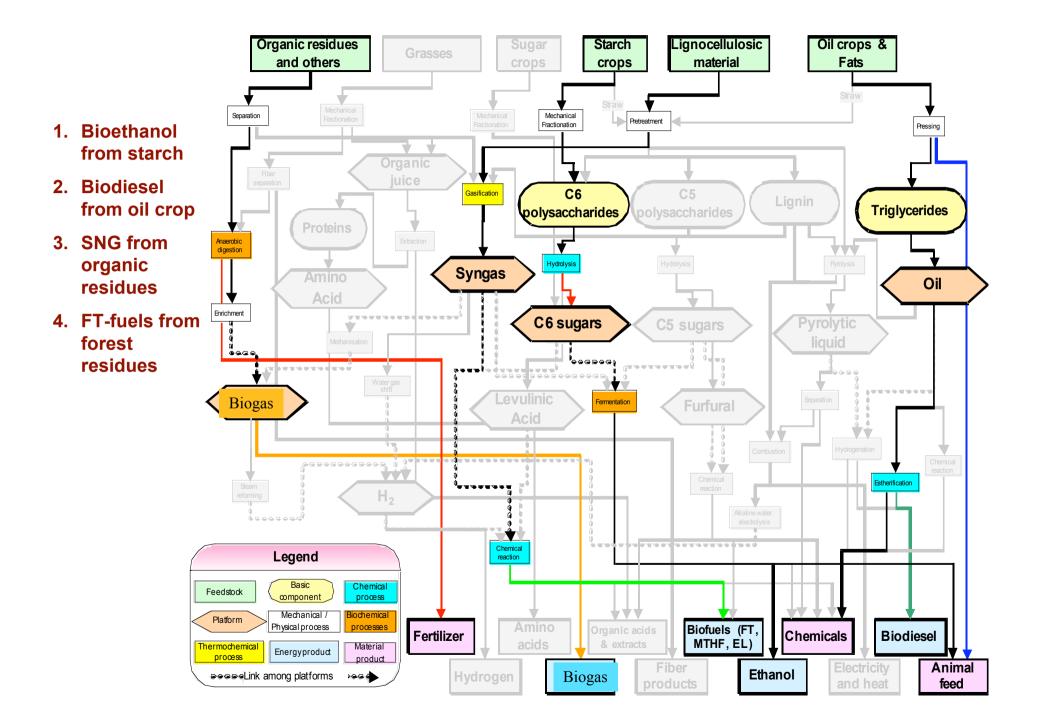
Identifying substates, intermediate products, and technological pathways

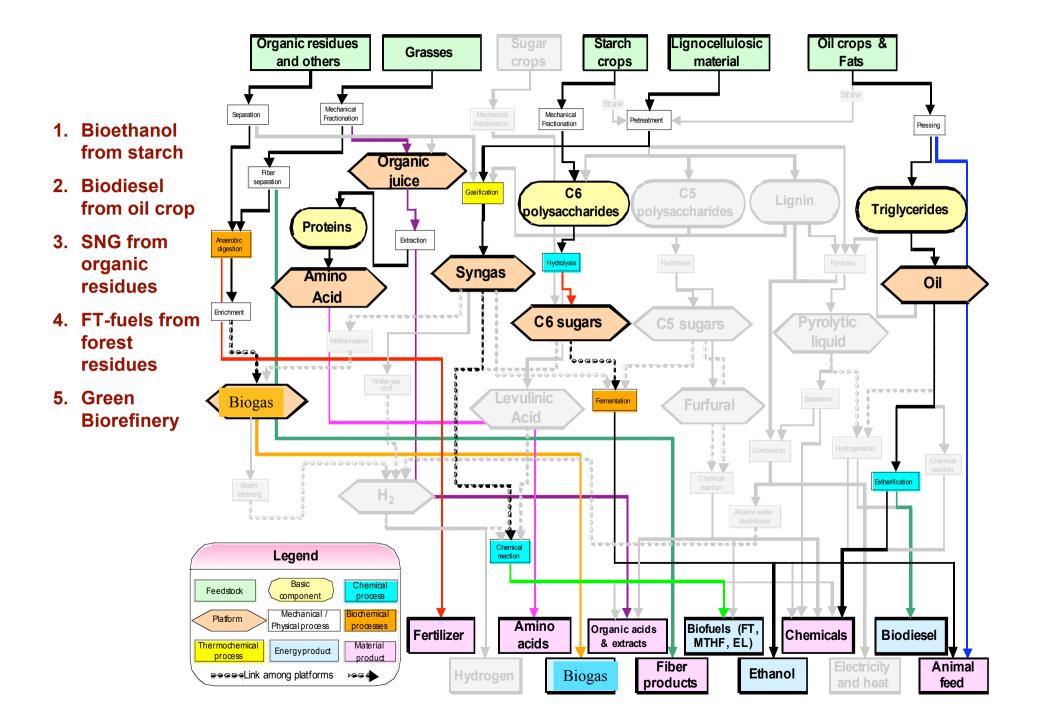


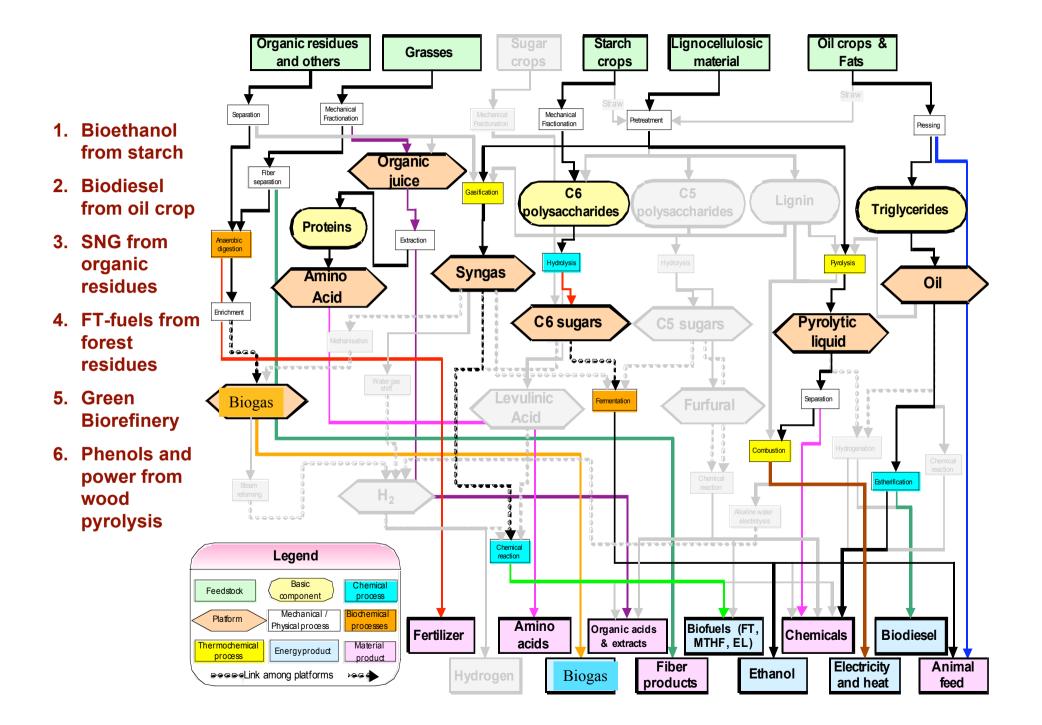


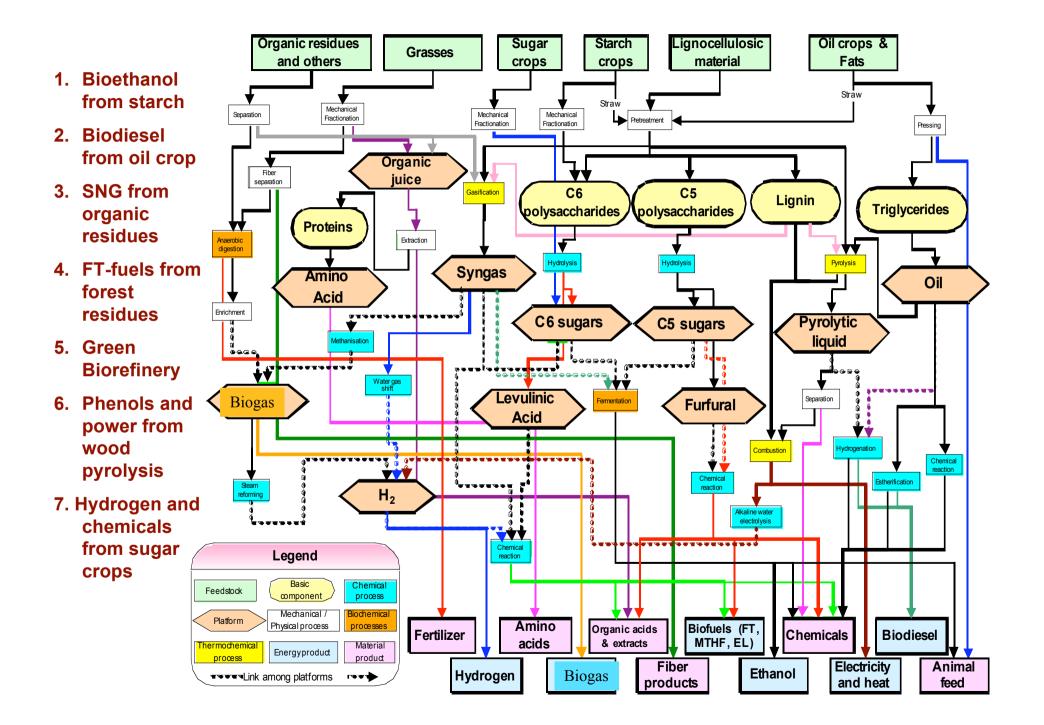




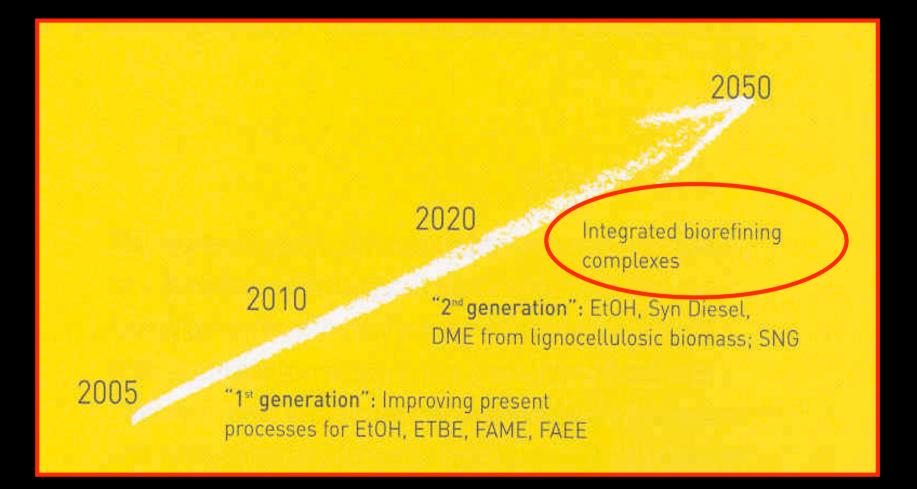








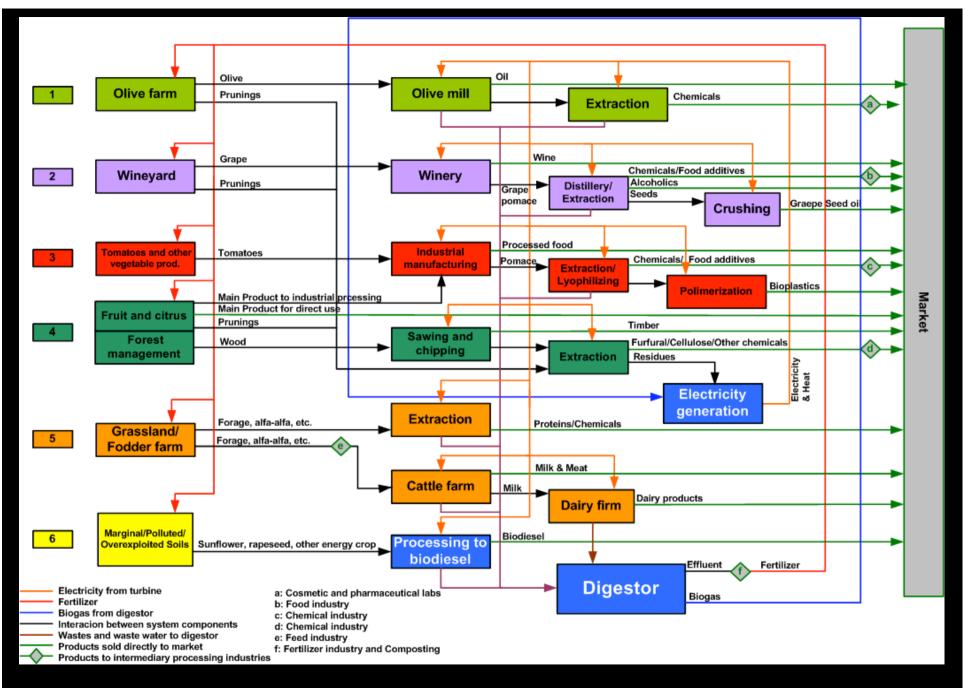
The European Union roadmap to Biorefineries (huge investments for research, 7th RTD program)



Source: Biofuels in the European Union – A vision for 2030 and beyond, Final report of the Biofuels Research Advisory Council, June 2006

Step No. 2:

Designing an integrated system



Agro-Industrial Integrated System "Parthenope" - Napoli, Italy

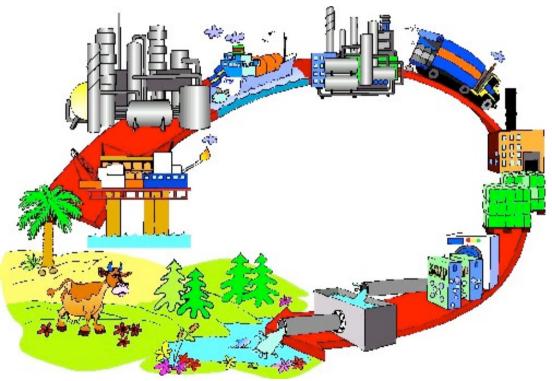
Step No. 3:

Assessing the profitability and environmental friendliness of biorefineries

A case study with LCA

Life Cycle Assessment- LCA

Life Cycle Assessment (LCA) is a technique for assessing the potential environmental aspects associated with a product (or service), by:



- compiling an inventory of relevant inputs and outputs
- evaluating the potential environmental impacts associated with those inputs and outputs
- interpreting the results of the inventory and impact phases in relation to the objectives of the study

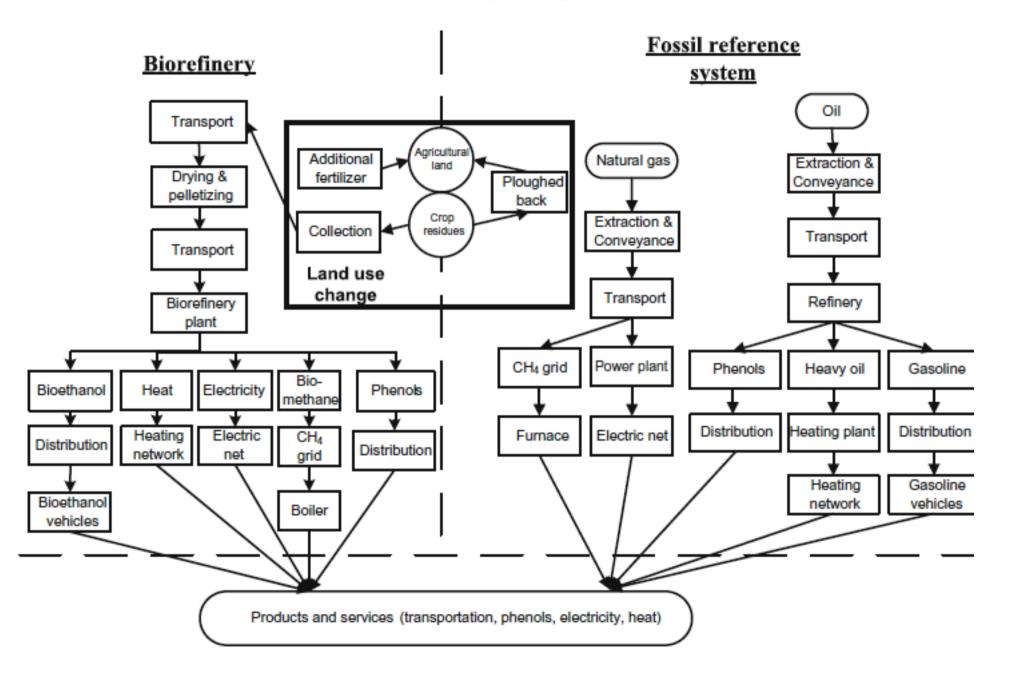


Fig. 1. Comparison between the production chains of the biorefinery and the fossil reference systems.

Table 4

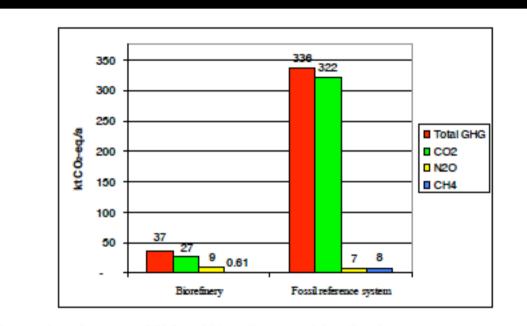
Final products produced from the biorefinery using com stover or wheat straw as raw materials,

Product	Unit/a	Biorefinery-Com stover	Biorefinery-Wheat straw
Bioethanol	10 ⁶ km	1208	1083
Heat (from biomethane)	TJ	243	350
Electricity (from CHP)	TJ	183	90,2
Heat (from CHP)	TJ	2.17	3.74
Phenols	kt	1.75	1,46



Table 6. Quantities of final products, GHG emissions and primary energy demand of biorefinery system and fossil reference system.

Birefinery System			Fossil Reference System		
Product/service:			Product/service:		
Transportation (bioethanol)	1,082	Mio km	Transportation (gasoline)	1,204	Mio km
Transportation (MTHF)	122	Mio km			
Furan resins	2.91	kt	Epoxy resins (from fossil)	2.91	kt
FUMA	3.34	kt	FUMA (from fossil)	3.34	kt
Electricity	333	TJ	Electricity (from natural gas)	333	TJ
Heat	224	TJ	Heat (from oil)	224	TJ
Biomethane	261	TJ	Natural gas	261	TJ
H2	13.7	TJ	H ₂ (from natural gas)	13.7	TJ
O2	7.07	kt	O2 (conventional, from air)	7.07	kt
Fertilizer (no benefit)	36.9	kt _{dry}			
Environmental impacts:			Environmental impacts (includi	ng beat):	
Total GHG emissions	36.8	kt CO ₂ -eq./a	Total GHG emissions	336	kt CO ₂ -eq./a
CO ₂	27.0	kt CO2-eq./a	CO ₂	322	kt CO ₂ -eq./a
N,O	9.22	kt CO ₂ -eq./a	N,O	7.27	kt CO ₂ -eq./a
CH4	0.61	kt CO ₂ -eq./a	CH4	7.69	kt CO ₂ -eq./a
Primary energy demand	10,858	TJ/a	Primary energy demand	4,772	TJ/a
Fossil	208	TJ/a	Fossil	4,736	TJ/a
Renewable (biomass)	10,495	TJ/a	Renewable	7	TJ/a
Others	16	TJ/a	Others	25	TJ/a
GHG and energy savings					
	eat credits		Environmental impacts (excludi	-	
GHG emissions saved	300	kt CO ₂ -eq./a	Total GHG emissions		kt CO ₂ -eq./a
	0.66	t CO2-eq./tdrywood	CO ₂	299	kt CO ₂ -eq./a
Fossil energy saved	4,527	TJ/a	N ₂ O	6.76	kt CO ₂ -eq./a
	10.05	GJ/t _{drywood}	CH ₄	7.15	kt CO ₂ -eq./a
Excluding	e he at credits				
GHG emissions saved	276	kt CO ₂ -eq./a	Primary energy demand	4,474	TJ/a
	0.61	t CO2-eq./tdrywood	Fossil	4,440	TJ/a
Fossil energy saved	4,231		Renewable	6	TJ/a
	0.20	GJ/t _{drywood}	Others	24	TJ/a



Comparison between GHGs of biorefinery and fossil reference system.

Table 5

GHG emissions and savings of the biorefinery systems in comparison with their respective fossil reference systems.

	Unit/a	Corn stover	Fossil reference system	Wheat straw	Fossil reference system
GHG emissions					
Total	kt CO2-eq.	137	296	130	255
CO ₂	kt CO ₂ -eq.	107	280	113	242
N2O	kt CO2-eq.	26,3	6,51	13,3	5.79
CH₄	kt CO2-eq.	3.89	10,5	3,88	7.7
GHG savings					
Per year	kt CO ₂ -eq.	159		125	
Per year	*	53.7		49.0	
Per t _{dry} feedstock	t CO ₂ -eq./t _{áry}	333		262	
Per hectare	t CO ₂ -eq./ha	3,01		1,82	

Table 6

Results of the CML impact assessment method.

Impact category	Unit	Biorefinery com stover	Fossil reference system	Biorefinery wheat straw	Fossil reference system
Abiotic depletion	kt Sb eq	0,30	2,09	0.35	1,78
Global warming (GWP100)	kt CO ₂ -eq	137	296	130	255
Ozone layer depletion (ODP)	kg CFC-11 eq	8.31	29.7	8.86	26,9
Human toxicity	kt 1,4-DB eq	24.7	192	25,6	167
Fresh water aquatic ecotox,	kt 1,4-DB eq	2.54	17.4	2,90	14.8
Marine aquatic ecotoxicity	Mt 1,4-DB eq	17.7	51,2	20.1	44.5
Terrestrial ecotoxicity	kt 1,4-DB eq	0.22	0,60	0,28	0.54
Photochemical oxidation	kt C ₂ H ₄	0.06	0,28	0.05	0.25
Acidification	kt SO ₂ eq	0.93	1,16	0.78	1.03
Eutrophication	kt PO ₄ -eq	0,52	0.17	0,39	0.15

Step No. 4 Expanding the focus of the assessment:

- a) thermodynamic efficiency (exergy),
 b) demand for environmental support (eMergy), and
- c) economic feasibility.

An extended LCA

Multidimensional Life Cycle Assessment



Matter and energy flows

2. Extended LCA: SUMMA

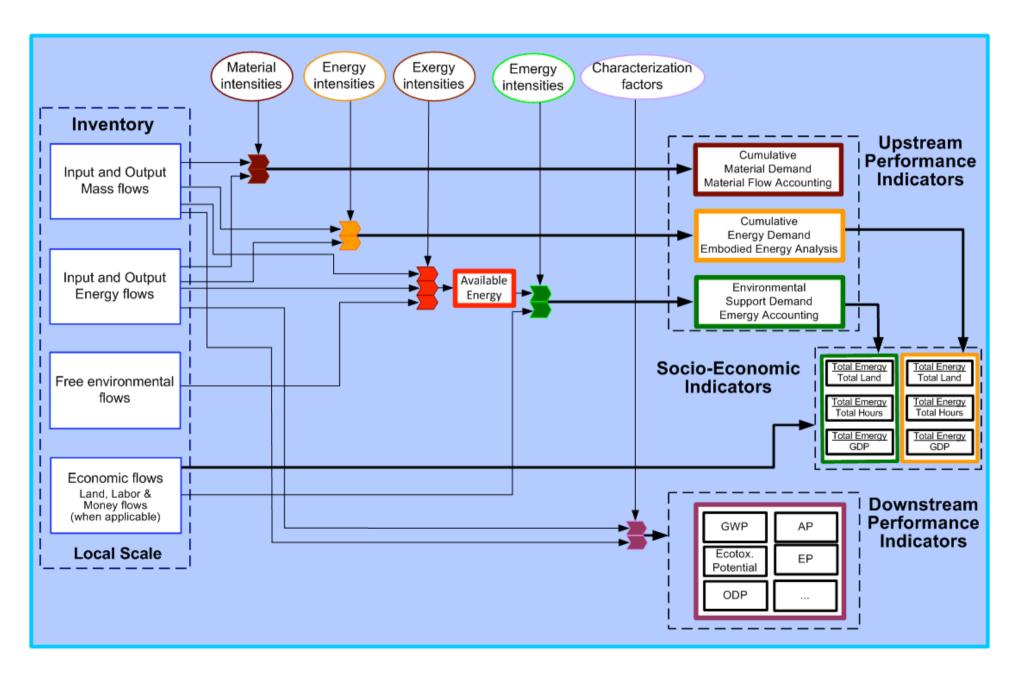
SUstainability Multimethod Multiscale Approach





LCA + process efficiency + environmental support + embodied time + money flows

SUstainability Multimethod Multiscale Approach



Step No. 5: Marginal and polluted land (GIS - Geographical Information System)

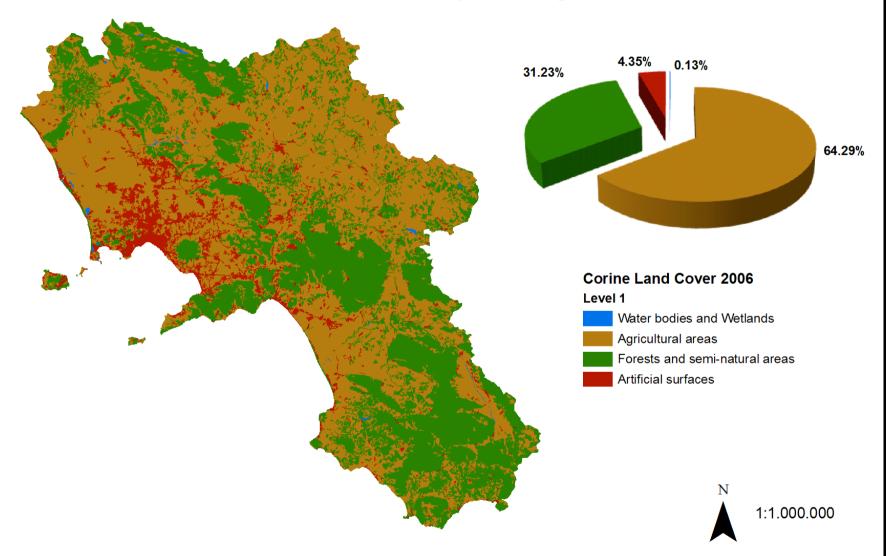
Case study:

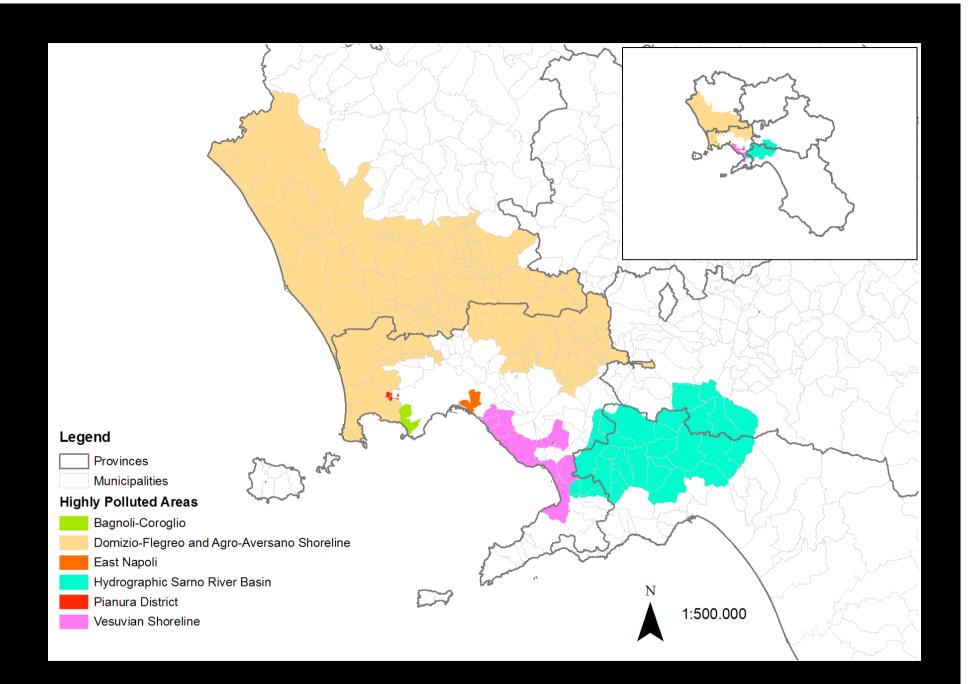
Non-food crops on land unsuitable for agriculture.

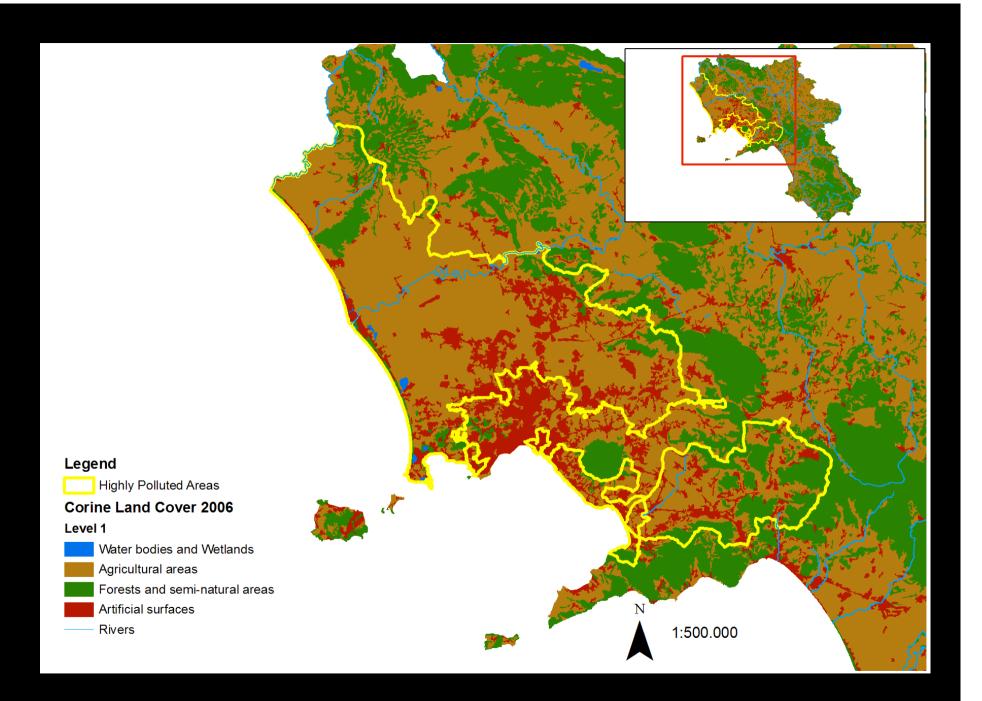
a) Cropping for energy

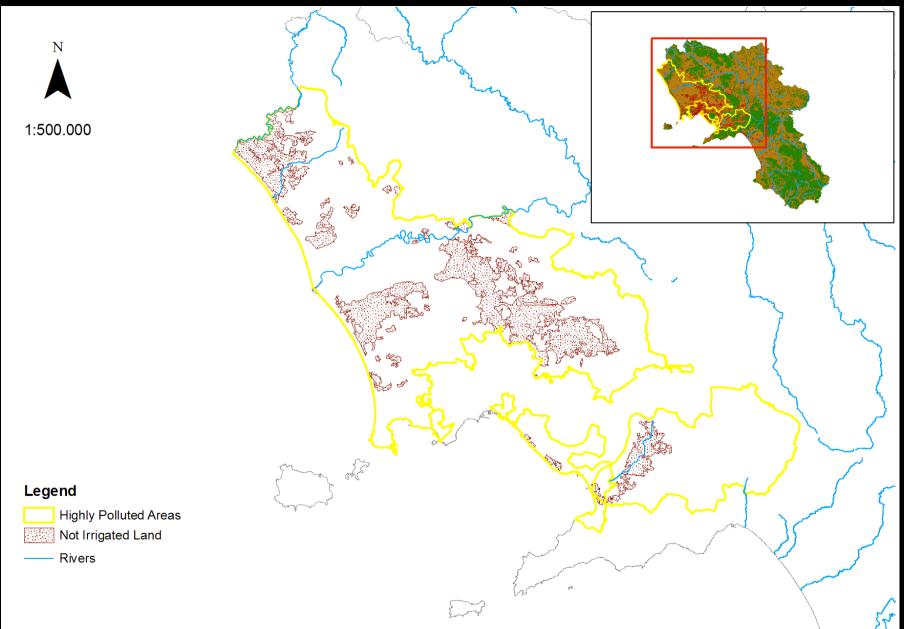
b) Biorefinery, the Biofine process

Land Use in Campania Region



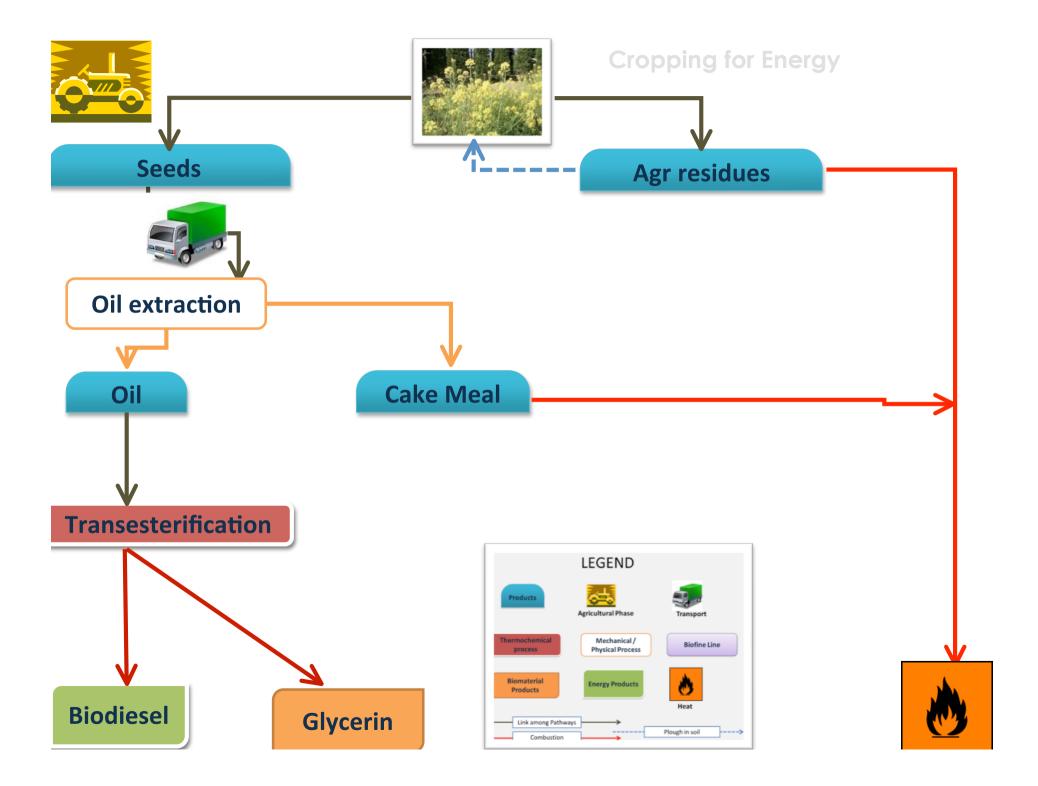






2. Ethiopian Mustard or Brassica carinata





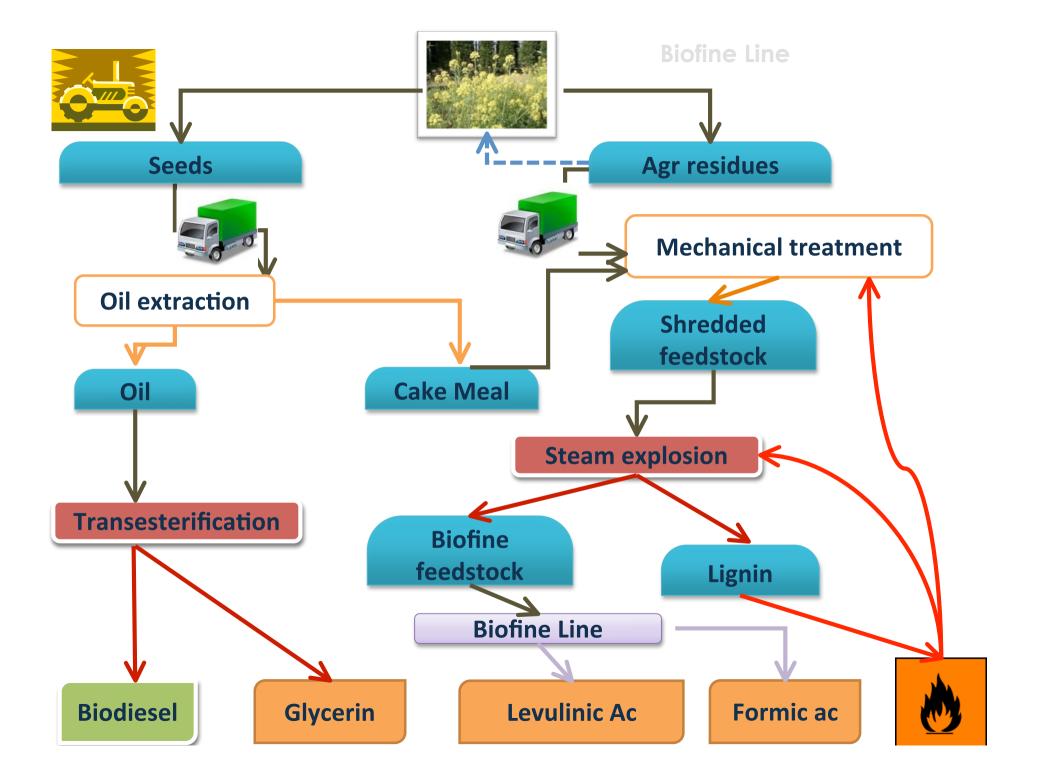
Usable and Net Energy Delivered to the user by all the co-products of the different									
phases of biodiesel production chain (data per hectare).									
		Energy content (J/ha/yr)	Usable Energy (for residues 50% less than HHV) (J/ha/yr)	Transportation of residues (5% of energy content) (J/ha/yr)	Usable Energy Delivered (J/ha/yr)	Net Energy Delivered (J/ha/yr)			
lt	Invested for process	1.82E+10							
Low Input	Biodiesel	1.46E+10	1.46E+10	7.30E+08	1.39E+10				
w I	Cake meal	1.17E+10	5.85E+09	5.85E+08	5.27E+09				
Lo	Straw	4.36E+10	2.18E+10	2.18E+09	1.96E+10				
	Delivered				3.88E+10	2.06E+10			
lt	Invested for process	2.59E+10							
ndu	Biodiese l	2.06E+10	2.06E+10	1.03E+09	1.96E+10				
High Input	Cake meal	1.66E+10	8.30E+09	8.30E+08	7.47E+09				
Hig	Straw	5.51E+10	2.76E+10	2.76E+09	2.48E+10				
	Deliver e d				5.19E+10	2.60E+10			
	I				1				

Net Energy Delivered (NED) by the biodiesel production chain and fractions of agricultural and regional energy consumption potentially replaced

	Low Input (J/yr)	High Input (J/yr)
Total NED from polluted areas	8.90E+14	1.12E+15
% of energy budget of Campania region	0.33%	0.41%
% of energy budget of regional agricultural sector	10.63%	13.41%

Economic balance between the total economic investment for biodiesel and heat production chain and the saving of economic investment associated to such bioenergy in marginal land.

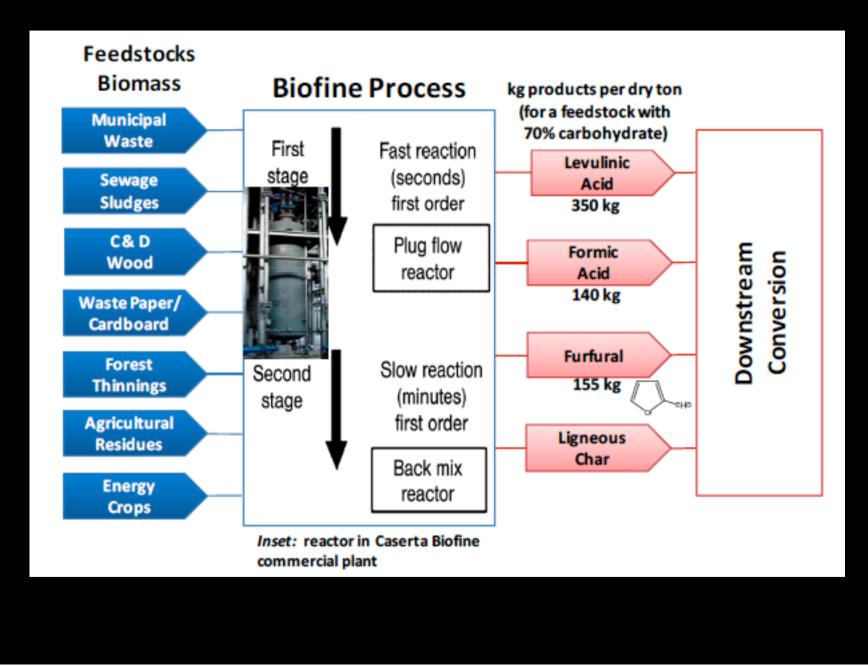
	Low Input (€/yr)	High Input (€/yr)
Total Economic Investment (a)	3.78E+07	4.62E+07
Value of delivered energy (b)	9.68E+06	1.22E+07
Economic Balance (b-a)	-2.81E+07	-3.40E+07
Ratio a/b	3.90	3.79

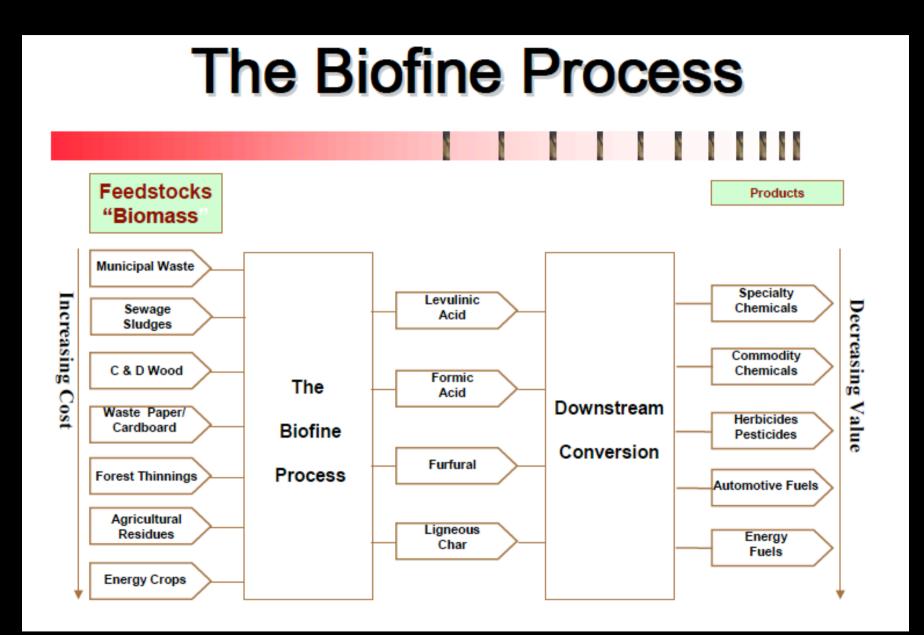


An Example: The Biofine Process

An Existing Process

- A high temperature, fast acid hydrolysis of biomass polysaccharides.
- The feedstock is hydrolysed with 1-5% sulphuric acid in two reactors.
- The first reactor hydrolyses the sugars and produces 5hydroxymethyl furfural (HMF) from the C6 sugars and furfural from the C5 sugars.
- The HMF goes to the second reactor where levulinic acid is formed (and smaller amounts of formic acid)





Products and by-products	% of extraction	Ref	Mass of product (kg ha ⁻¹ yr ⁻¹)	Total mass () (kg yr ⁻¹)	Market Price (€ kg ⁻¹)	Ref	Total value (€)
Seeds (*)			1200.00	5.18E+07			
Oil ()	33.0%	[58]	396.00	1.71E+07			
Lubrificants (*)	6.0%	[58]	23.76	1.03E+06	0.88	[62]	9.03E+05
Biodiesel (*)	98.0%	[58]	388.08	1.68E+07	0.78	[62]	1.31E+07
Glycerin (^d)	10.0%	[58]	38.81	1.68E+06	0.11	[62]	1.76E+05
Cake Meal (^b)	58.0%	[63]	696.00	3.01E+07			
Proteins (*)	39.0%	[63]	271.44	1.17E+07	1.60	[64]	1.88E+07
Fibers (*)	31.8%	[63]	221.33	9.56E+06	0.11	[65]	1.05E+06
Glucosinates (*)	5.1%	[63]	35.50	1.53E+06			0.00E+00
Soluble sugar (*)	5.7%	[63]	39.67	1.71E+06	2.40	[64]	4.11E+06
Others (*)	18.4%	[63]	128.06	5.53E+06			
Agricultural residues (*)			3400.00	1.47E+08			
Cellulose (
Glucose	32.5%	[66]	1105.00	4.77E+07	0.30	[64	1.43E+07
Hemicellulose (⁶)							
Xylose	18.0%	[66]	612.00	2.64E+07	3.50	[67]	9.25E+07
Galactose	1.5%	[66]	51.00	2.20E+06	n .a.		
Arabinose	1.2%	[66]	40.80	1.76E+06	n .a.		
Mannose	1.2%	[66]	40.80	1.76E+06	n .a.		
Lignin (⁶)	18.7%	[66]	635.80	2.75E+07	0.20	[68]	5.49E+06
Others (*)							
Ash	5.2%	[66]	176.80	7.63E+06			
Extractives	20.9%	[66]	710.60	3.07E+07			
Total economic income from	biorefinery ch	ain	•	•	· · ·		1.50E+08

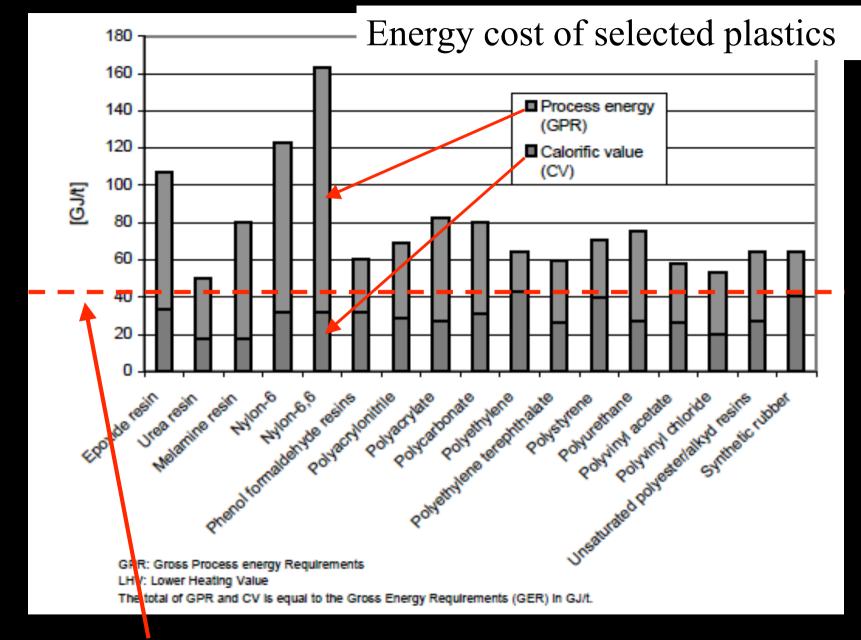
() Referred to 43183 ha of Brassica cropping; (*) from Brassica cropping; (*) from seeds; (*) % of oil mass, (*) % from biodiesel; (*) from cake meal mass; (*) from agricultural residues

Economic balance between the total economic investment for biorefinery chain and total production income.

Total economic investment for energy purpose (€/yr)	2.87E+07
Cost for biorefinery plant (€/yr)	4.26E+07
Total cost (a) (€/yr)	7.13E+07
Economic income from biorefinery chain (b) (€/yr)	1.50E+08
Net economic (b-a) (€/yr)	7.90E+07
Ratio b/a	2.11

Indicators	Levulinic Acid	Formic Acid	Biodiesel	Glycerin				
Material resource depletion								
MI abiot (g/g)	4.48	0.37	2.68	1.19				
MI water (g/g)	26.17	2.17	27.56	12.20				
Energy depletion								
GER per unit mass (J/g)	3.29E+04	2.73E+03	2.08E+04	9.19E+03				
Oil eq (g oil/g)	0.78	0.07	0.50	0.22				
Oil eq (g oil/J)	2.20E-05	8.13E-06	1.32E-05	1.32E-05				
Oil eq (g oil/€)	871	871	633	2090				
Emergy (demand for environmental support)								
Specific emergy (seJ/g)	3.58E+12	1.24E+13	1.17E+10	1.17E+11				
Transformity (seJ/J)	9.83E+07	1.51E+09	3.11E+05	7.02E+06				
EYR	1.00	1.00	1.14	1.14				
ELR	56.87	56.87	8.28	8.28				
% Renewable	2%	2%	11%	11%				
Climate change								
Global warming (g CO2 -equiv/ g)	2.46	0.20	1.24	0.55				
Acidification (g SO2 / g)	9.66E-03	8.02E-04	3.92E-03	1.73E-03				
Eutrophication (g PO4/g)	9.44E-04	7.84E-05	4.10E-04	1.82E-04				

42 GJ/ton: approx energy content of raw oil





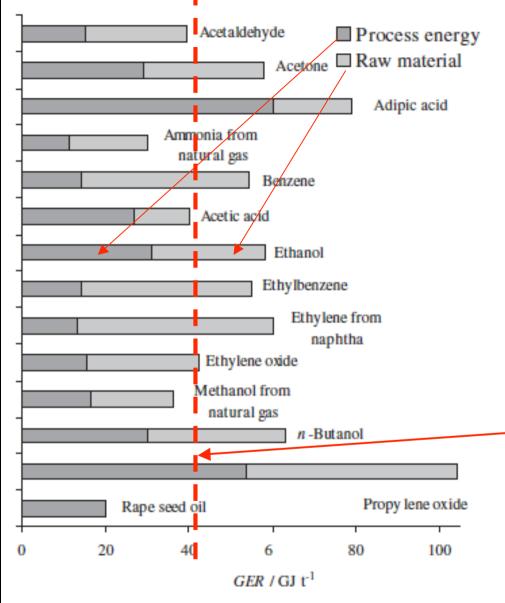


Fig. 4. Gross energy requirements (GER) for important base chemicals [18,19].

Energy cost of selected chemicals

Approx energy content of raw oil: 42 GJ/ton:

Concluding remarks

- We will have to rely on biomass for liquid fuels, chemicals and materials, when we run out of cheap fossil fuels. No doubt on this.
- Cropping for energy, even in marginal land, is never an option (a part from Brazilian sugar cane, in some cases) due to low energy return and high costs.
- Instead of expensive cropping, the use of lignocellulose residues and waste provides interesting, substrate abundant, low cost and energy self-sufficient alternatives (biorefinery).
- The biorefinery concept solves the problem of agro-industrial and urban waste, and promises cheap liquid fuels and biomaterials/biochemicals.
- Biochemicals can be already produced at competitive cost with petrochemicals. Bioenergy is more difficult, because of low hydrolysis yields.
- Some high yield processes (Biofine) are very close to the commercial stage.
- Lignocellulose is everywhere and therefore contributes to the independence from fossil fuels.

Thank you for your attention!